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Quick scan Jababeka Industrial Estate

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COOPERATING COMPANIES & UNIVERSITIES





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1 PREFACE

1.1 INTRODUCTION

The main focus of work package 3 of the Geocap programme is direct use of low and medium enthalpy in West Java. Based on subsurface potential and surface demand, Jababeka Industrial Estate is a potentially interesting location.

1.2 OBJECTIVE

The objective of the study is to investigate the feasibility on a quick scan level on technical and financial aspects.

1.3 RESULTS

The results of the quick scan are presented in this report. The following chapters will describe in more detail the starting points, geology, concepts, analysis of concepts and the conclusions and recommendations.



2 STARTING POINTS

2.1 LOCATION

Jababeka Industrial Estate is a modern eco-industrial estate, situated in Bekasi. It spans more than 2,000 hectares and has more than 1,650 local and international companies. The power plant of Cikarang Listrindo supplies power to the estate.



Figure 1: Location of Jababeka Industrial Estate (orange circle)

2.2 HEAT DEMAND

2.2.1 Potential heat customers

In a desktop study, the following potential heat customers has been identified:

- Unilever
- L'Oréal
- Fajar Paper

The potential heat customers are shown in Figure 2.





Figure 2: Location potential heat customers

2.2.2 Heat demand

Energy consumption of the potential heat customers is confidential, it could not be obtained for this quick scan. Based on available knowledge and expertise, the required heat temperature and capacity are estimated. These are shown in Table 1.

| Customer | Туре | Temperature | Capacity | Demand |
|-------------|-------------------------|-------------|----------|---------|
| | | [°C] | [MWt] | [MWht] |
| Unilever | Food and consumer goods | 100 | 15 | 120,000 |
| L'Oreal | Consumer goods | 70 | 10 | 80,000 |
| Fajar Paper | Pulp and paper | 110 | 10 | 80,000 |
| Fajar Paper | Pulp and paper | 160 | 25 | 200,000 |

Table 1: Estimated heat capacity and demand



2.3 OTHER PARAMETERS

Other parameters are shown in Table 2. Values are estimated.

| Parameter | Unit | Value |
|-------------------|---------|-------|
| Electricity price | \$/MWhe | 75 |
| Steam price | \$/ton | 25 |
| Heat price | \$/MWh | 30 |

Table 2: Financial and economical parameters



3 GEOLOGY

In the resource assessment a detailed study of the potential of the West Java Basin was made. This chapter shows the results for the estimated depth, temperature, flow rate and thermal power. For more details, the reader is referred to the full Geocap Resource Assessment report.

3.1 AQUIFER DEPTH AND THICKNESS

The depths to the top of Baturaja and Talang Akar aquifers and their thicknesses are obtained from PT LAPI ITB (2014) report, as well as Suryantini (2007) for wells whose depth and thickness values are not reported in the former. If a well does not possess values from any of the two references, the values obtained from the 3-D geological model of the onshore North West Java Basin constructed by Putra (2015) are used. Since the thickness values adopted from the last two references are of the entire sequence of the Lower Cibulakan Formation, the thickness of each aquifers derived from these references is equal to half of the Lower Cibulakan's. The depth and thickness values are listed in Table 3, while the spatial distribution of the depth is represented in maps shown in Figure 3 and Figure 4.

| Well | Baturaja | | Talang Akar | |
|------|-----------|---------------|-------------|---------------|
| | Depth (m) | Thickness (m) | Depth (m) | Thickness (m) |
| ССН | 2550 | 300 | 2850 | 300 |
| JTN | 1280.5 | 371 | 1612 | 292 |
| CKR | 2124.5 | 289 | 2413.5 | 289 |
| PDM | 2007 | 298 | 2336.5 | 357 |
| PDT | 1871.1 | 237 | 2101.1 | 223 |
| RJW | 1800 | 200 | 2000 | 200 |
| GLN | 1350 | 150 | 1500 | 150 |
| TBN | 1403.25 | 145.5 | 1498 | 44 |
| CPD | 1600 | 200 | 1800 | 200 |
| KRW | 2370 | 250 | 2620 | 250 |
| KRK | 2025 | 250 | 2275 | 250 |
| RDK | 1302.7 | 112 | 1414.7 | 112 |
| TNG | 1075 | 150 | 1225 | 150 |

Table 3 Tabulated depth-to-centre and thickness values of the Baturaja and Talang Akar aquifers. Black-coloured values denote those obtained from PT LAPI ITB (2014). Blue-coloured values indicate those taken from the geological model used by Putra (2015). Red-coloured values denote those obtained from Suryantini (2007).



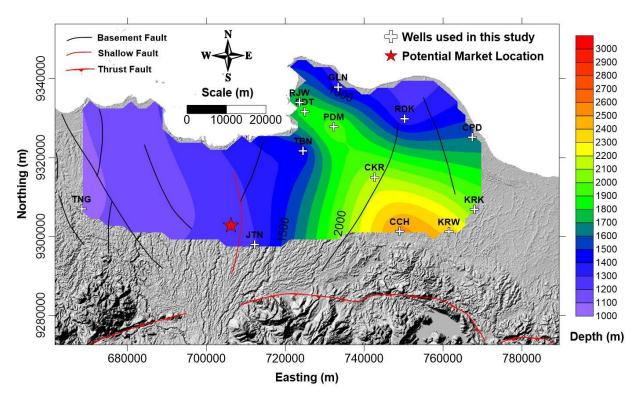


Figure 3 Map showing the distribution of depth to the centre of Baturaja aquifer.

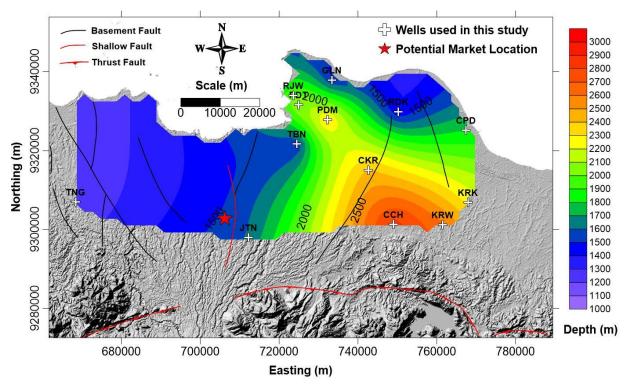


Figure 4 Map showing the distribution of depth to the centre of Talang Akar aquifer.



3.2 AQUIFER TEMPERATURE

The temperatures were calculated at the centre of Baturaja and Talang Akar aquifers at different locations. For locations at which the temperature gradient value (i.e. that obtained from PT LAPI ITB, 2014) at the particular depth interval of the formation does not exist, the modelled temperature of Putra (2015) was used. The calculated temperatures are listed in Table 4, while the aquifer temperature maps are given in Figure 5 and Figure 6.

| Well | Temperature (°C) | | |
|------|------------------|-------------|--|
| | Baturaja | Talang Akar | |
| ССН | 152.61 | 168.29 | |
| JTN | 96.93 | 108.49 | |
| CKR | 91.9 | 117.2 | |
| PDM | 110.19 | 119.2 | |
| PDT | 94.12 | 102.61 | |
| RJW | 117.6 | 125.63 | |
| GLN | 62.69 | 68.13 | |
| TBN | 59.98 | 64.71 | |
| CPD | 92.8 | 106.9 | |
| KRW | 85.11 | 95.74 | |
| KRK | 90.23 | 100.54 | |
| RDK | 61.7 | 65.45 | |
| TNG | 46.51 | 49.1 | |

Table 4 Tabulated temperature within the Baturaja and Talang Akar aquifers. Black-coloured values denote those calculated using thermal gradients derived from temperatures collated in PT LAPI ITB (2014). Blue-coloured values indicate those taken from the modelled temperature of Putra (2015).



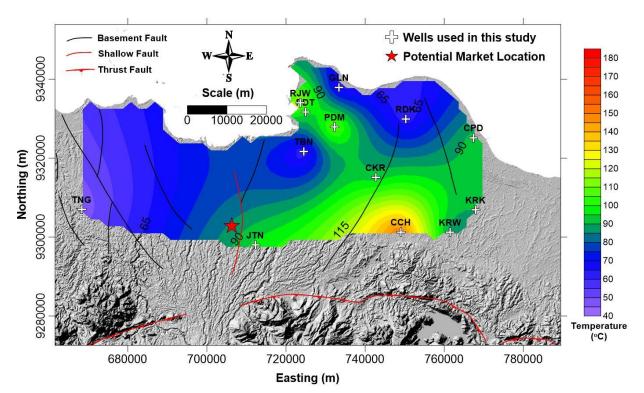


Figure 5 Map showing the distribution of temperatures within the Baturaja aquifer.

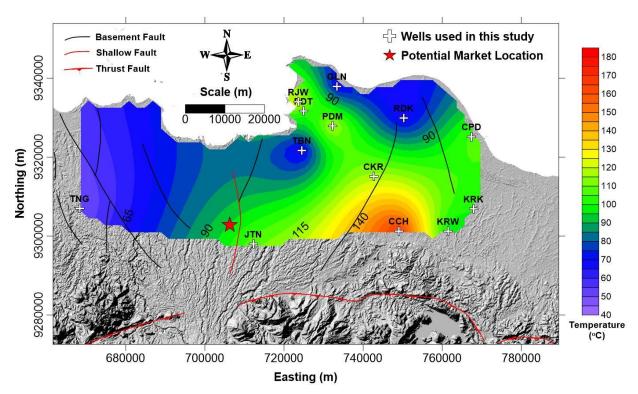


Figure 6 Map showing the distribution of temperatures within the Talang Akar aquifer.



3.3 CALCULATION OF FLOW RATE AND THERMAL POWER

The flow rate and thermal power of each well were calculated and presented in Table 5. A map was also constructed for the latter (Figure 7 and Figure 8).

| Well | Batu Raja | | Talang Akar | |
|------|-----------|---------------|-------------|---------------|
| | Flow Rate | Thermal Power | Flow Rate | Thermal Power |
| | (m³/h) | (MW) | (m³/h) | (MW) |
| ССН | 578.8 | 79.14 | 651.7 | 100.32 |
| JTN | 320.2 | 24.22 | 373.9 | 33.02 |
| CKR | 296.8 | 20.81 | 414.4 | 40.56 |
| PDM | 381.8 | 34.43 | 423.6 | 42.39 |
| PDT | 307.2 | 22.29 | 346.6 | 28.37 |
| RJW | 416.2 | 40.92 | 453.5 | 48.58 |
| GLN | 161.1 | 6.13 | 186.4 | 8.21 |
| TBN | 148.6 | 5.21 | 170.5 | 6.87 |
| CPD | 301.0 | 21.40 | 366.5 | 31.73 |
| KRW | 265.3 | 16.62 | 314.7 | 23.39 |
| KRK | 289.1 | 19.74 | 337.0 | 26.82 |
| RDK | 156.5 | 5.79 | 174.0 | 7.15 |
| TNG | 86.0 | 1.75 | 98.0 | 2.27 |

Table 5 Calculated flow rate and thermal power of the Baturaja and Talang Akar aquifers.



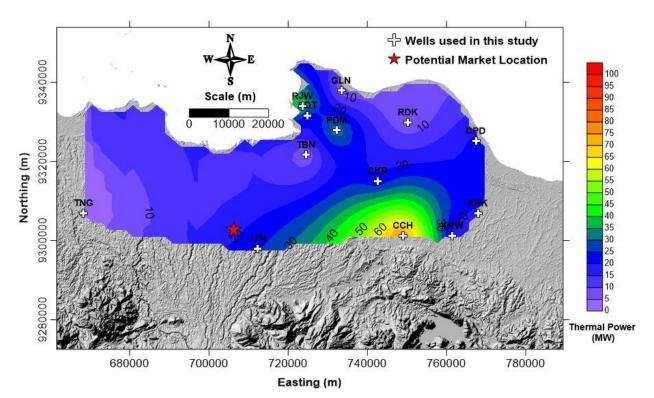


Figure 7 Map showing the distribution of calculated well thermal power of the Baturaja aquifer.

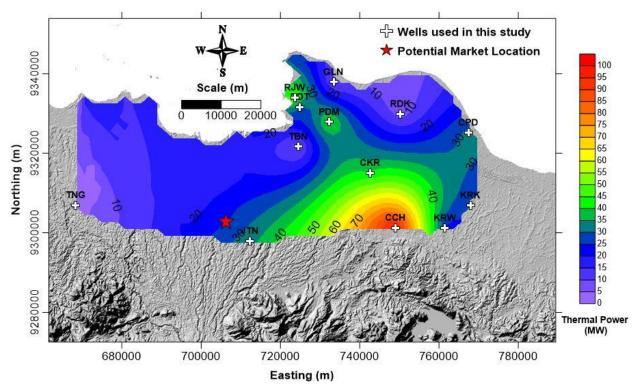


Figure 8 Map showing the distribution of calculated well thermal power of the Talang Akar aquifer.



Using these results, the depth, flow and temperature at Jababeka Industrial Estate are estimated (see Table 6).

| Well | Unit | Value |
|-------------|------|-------|
| Depth | mTVD | 2,600 |
| Flow | m3/h | 400 |
| Temperature | °C | 135 |

Table 6 Estimated potential West Java Basin at Jababeka Industrial Estate



4 ENERGY CONCEPTS

4.1 CONCEPT 1: HOT WATER AT 100°C

Concept 1 is shown schematically in Figure 9. Geothermal brine is used to produce hot water. Using a heating grid, hot water is transported to Unilever and l'Oréal, where it can be used for all kinds of processes that have a heat demand. For now, it is assumed that hot water can be used without making any adjustments to the heating system at Unilever and l'Oréal. Fajar paper is not connected because it is expected that they only require steam.

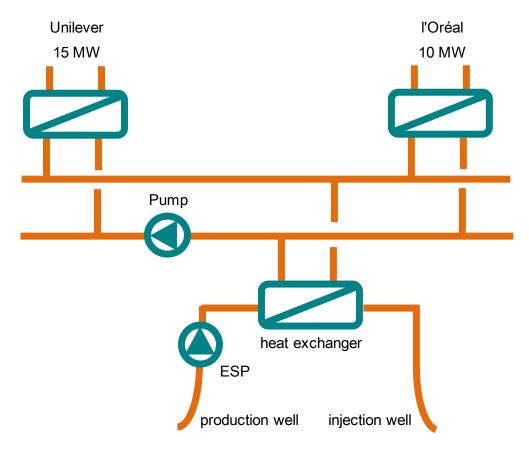


Figure 9: Schematic overview concept 1: hot water at 100°C

Geothermal system

Hot brine is extracted out of the production well. The temperature of the brine is expected to be 130°C (see chapter 3). In a heat exchanger, heat is transferred to the heating grid. The brine will cool down and is injected in the injection well. An electric submersible pump (ESP) is necessary to inject the brine. A typical coefficient of performance (COP) of an ESP is 15. This means that to for every 15 kWh of extracted thermal energy, 1 kWh is used by the ESP.



4.2 CONCEPT 2: STEAM AT 110°C

Concept 2 is shown schematically in Figure 10. As in concept 1, heat is transported using a heating grid. Fajar Paper, Unilever and l'Oreal are connected to the heating grid. At each industrial location, a steam heat pump is used to produce steam at a temperature of 110°C. It is assumed that this steam can be used without making any other changes to the heating system.

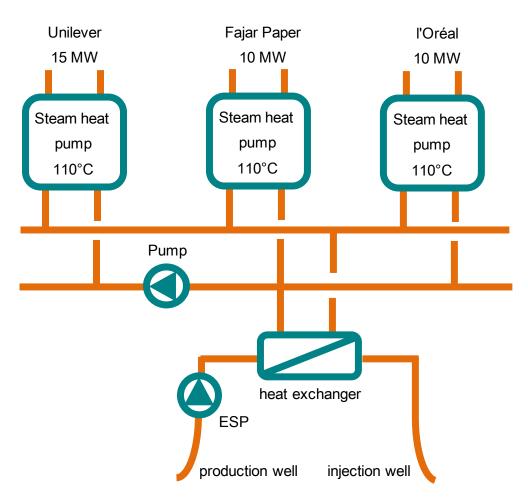


Figure 10: Schematic overview concept 2: steam at 110°C

Steam heat pump 110°C

In a steam heat pump, water is evaporated, creating steam. Steam heat pumps up to 120°C are commercially available. In this case, the COP is estimated at 4,5.



4.3 CONCEPT 3: STEAM AT 160°C

Concept 3 is shown schematically in Figure 11. In this concept, only Fajar Paper is connected to the geothermal system. It is estimated that the total heat demand of Fajar Paper is equal to the geothermal capacity. Multiple heat pumps are used to produce steam at 160°C. It is assumed that this steam can be used without making any other changes to the heating system.

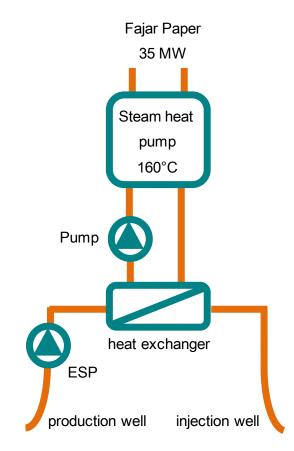


Figure 11: Schematic overview concept 3: steam at 160°C

Steam heat pump 160°C

To make steam at 160°C, a two-stage steam heat pump is required. At this moment, a steam heat pump up to 160°C is still in development. ECN (Dutch Energy Research Centre) for example is testing an experimental steam heat pump. The results so far are promising and the expectation is that the product will come to market in the near future. In this case, the COP is estimated at 3,4.



5 ANALYSIS

5.1 ENERGY & SUSTAINABILITY ANALYSIS

For each concept, the primary energy consumption is calculated. This energy consumption is compared to a conventional concept, in which case hot water and steam are generated with gas fired boilers. A summary is given in Figure 12.

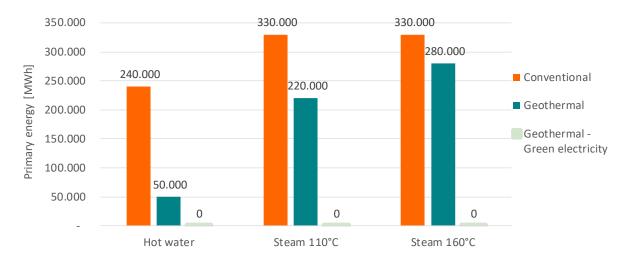


Figure 12: Primary energy consumption per year for concepts

In all cases, the geothermal concept require less primary energy than the conventional situation. The primary energy reduction can be decreased further by using green electricity. In the geothermal concept with a steam heat pump, the primary energy savings are more limited. The electricity consumption is relatively high, due to required compressors in the steam heat pump.

Using the primary energy consumption as shown in Figure 12, the CO_2 emissions are calculated. The results are shown Figure 13.



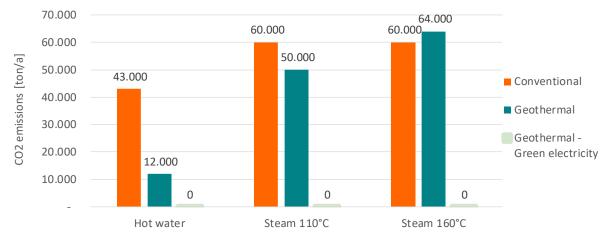


Figure 13: CO₂ emissions per year for concepts

For hot water production, there is a significant CO2 reduction. In case of 110°C steam, there is a limited CO2 reduction. In case of 160°C steam production, there is actually an increase in CO2 emissions, due to the high electricity consumption of the steam heat pump. Using green electricity, there are no CO2 emissions.

Concluding remarks

Using geothermal heat to produce hot water will greatly reduce CO2-emissions. Energy consumption is very limited due to direct heat transfer. When a steam heat pump is required, the electricity consumption will increase significantly due to the compressors needed. Using geothermal heat, CO2 emissions will only be reduced up to low steam temperatures (110°C). Producing geothermal steam at 160°C is not recommended, because this will increase CO2 emissions. Note however that the CO2 emission can be reduced by using green electricity.

5.2 FINANCIAL ANALYSIS

For all concepts, the investment costs, exploitation cost and revenues have been estimated on a quick scan level. To estimate the costs and revenues, general indicators are used. Values used can be found in Appendix 1. Also, the Payback Period (PP) is calculated, using the estimated cost and revenues. The results are shown in Table 7.



| CAPEX | | Hot water | Stem 110°C | Steam 160°C |
|-------------------------|---------|------------|------------|-------------|
| Geothermal | \$ | 18,900,000 | 18,900,000 | 18,900,000 |
| Insurances | \$ | 1,700,000 | 1,700,000 | 1,700,000 |
| Heat pump | \$ | - | 17,900,000 | 16,300,000 |
| Grid | \$ | 5,300,000 | 7,600,000 | 3,300,000 |
| Design & Consultancy | \$ | 2,600,000 | 4,600,000 | 4,000,000 |
| TOTAL | \$ | 28,500,000 | 50,800,000 | 44,300,000 |
| OPEX | | | | |
| Electricity | \$/year | 1,300,000 | 5,600,000 | 7,100,000 |
| Maintenance & operation | \$/year | 600,000 | 1,400,000 | 1,300,000 |
| TOTAL | | 1,900,000 | 6,900,000 | 8,300,000 |
| REVENUES | | | | |
| Heat/steam | \$/year | 6,000,000 | 11,000,000 | 11,000,000 |
| BUSINESS CASE | | | | |
| INCOME | \$/year | 4,100,000 | 4,000,000 | 2,600,000 |
| PP | \$/year | 7 | 13 | 17 |

Table 7 Estimated costs and revenues

Concluding remarks

The hot water case and 110°C steam case have a payback period less than the technical life span of the main components (the heat pump has a life time of 15 years while the geothermal wells have a life time of 30 years or more). However, for industry, the calculated payback periods are not interesting. In many cases, this has to be below 3 years. In case of renewable energy, 7 years might be negotiable, but 13 and 17 years are too long for industry. It is recommended to focus on a hot water case for industry on one hand, and on the other hand look for options on how to decrease the payback period for the 110°C steam case. For now, it Is not recommended to pursue the 160°C steam case.



6.1 CONCLUSIONS

- Jababeka Industrial Estate has a high geothermal potential. The potential of the West Java basin is estimated at 400 m3/h with a temperature of 135°C at a depth of 2,600 m.
- A heating grid can be used to transport geothermal heat to several end users. There it can be used for hot water production or for steam production.
- Using geothermal heat for hot water and 110°C steam production, CO2 emissions are reduced. In case of steam production, it is recommended to sue green electricity to boost the CO2 reduction.
- Geothermal hot water production has e payback period of 7 years. This might be negotiable with industry.
- Geothermal 110°C steam production has a payback period of 13 years. For industry, this is not interesting.

6.2 RECOMMENDATIONS

 It is recommended to contact industry at Jababeka, to share the results of this quick scan and try to get them involved in bringing this project a step further. Either hot water production, 110°C steam production or a combination of both could be interesting options.



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- PT LAPI ITB. 2014. Quick Scan: Early Investigation into Hot Sedimentary Aquifer Resource for Geothermal Cooling System Application in PERTAMINA Energy Tower Building. Project Report.
- Putra, S.D.H. 2015. Numerical Modeling of 3-D Conductive Subsurface Temperature Distribution and Its Applications to the Interpretation of Thermal Regime and Thermal Energy Estimation of the Onshore North West Java Basin. Unpublished Master's Thesis, Institut Teknologi Bandung, Indonesia.
- Suryantini. 2007. Determination of Heat Flow Values and Thermal Modeling of Western Java – Indonesia. Unpublished Doctoral Thesis, Kyushu University, Japan.



Appendix 1 KEY FIGURES

| Parameter | Unit | Value | Remarks | |
|-------------------------------|----------|--------|---------------------|--|
| Efficiency | | | | |
| COP geothermal system | - | 15 | | |
| COP steam heat pump 110°C | - | 5,1 | | |
| COP steam heat pump 160°C | - | 3,6 | | |
| COP heating grid | - | 50 | | |
| Investment | <u>.</u> | · | | |
| Geothermal system | \$/mTVD | 7,300 | | |
| Steam heat pump 110°C | \$/kWt | 500 | 11.7 MW per unit | |
| Steam heat pump 160°C | \$/kWt | 460 | 17.5 MW per unit | |
| Heating grid | \$/m | 1,100 | | |
| Integration cost heating grid | \$/MWt | 45,000 | | |
| Design and consultancy | - | 10% | of total investment | |
| Maintenance & operation (M&O) | | | | |
| M&O heating grid | - | 1% | of investment | |
| M&O geothermal system | - | 3% | of investment | |
| M&O steam heat pump | - | 4% | of investment | |

